

**Research Report** 

#### Non-Local, Memory-Dependent Fractional Diffusion in Nano-Porous Reservoirs

Erdal Ozkan, Colorado School of Mines



### **Problems in Flow Modeling and a Solution**

From a fundamental perspective, a major cause of the modeling and characterization problems in nano-porous formations is the inadequacy of the traditional perceptions to describe the movement of fluid molecules in

- extremely small confinement
- spatially disordered media and
- the fractal geometry of the cascade and the scales of natural fractures

Recently, <u>anomalous diffusion</u> has received attention in the context of stochastic physics to describe many physical scenarios similar to those in unconventional reservoirs



## Diffusion

Diffusion is the result of the random Brownian motion of individual particles.

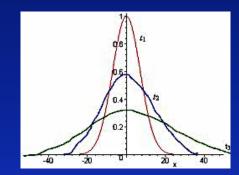
The mean square displacement of a particle is a linear function of time

 $\sigma_r^2 \sim Dt$ 

For the Brownian motion, the probability density function in space, evolving in time, is of the Gaussian type

This is a presumption of the use of Laplacian operator







### Background

## **Anomalous Diffusion**

However, a convincing number of works have indicated anomalous diffusion in which the mean square variance grows faster (superdiffusion) or slower (subdiffusion) than that in a Gaussian diffusion process.

Thus, a general relationship between the mean square variance and time is given by

$$\sigma_r^2 \sim Dt^{\alpha}$$

- $\alpha$  = 1 Normal Diffusion
- $\alpha \neq$  1 Anomalous Diffusion:
- $\alpha > 1$  Superdiffusion
- $\alpha$  < 1 Subdiffusion.

UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

### **Physical & Mathematical Basis**

## **Modeling Diffusion**

Fick's first law (diffusive flux) for one dimensional diffusion

$$J_C = -D\frac{\partial C}{\partial x}$$

Fick's second law (continuity equation):

$$\frac{\partial C}{\partial t} = -\frac{\partial}{\partial x} \left( J_C \right) = \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right)$$

**Defining scaled variables** 

$$x_D = x/x_0$$
  $t_D = t/t_0$   $C_D = C/C_0$ 

where  $x_0$ ,  $t_0$ , and  $C_0$  are the characteristics scales, we have

$$\left(\frac{x_0^2}{t_0}\right)\frac{\partial C_D}{\partial t_D} = \frac{\partial}{\partial x_D}\left(D\frac{\partial C_D}{\partial x_D}\right)$$



UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

### **Physical & Mathematical Basis**

# **Modeling Diffusion**

Dimensional

Dimensionless

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right) \qquad \qquad \left( \frac{x_0^2}{t_0} \right) \frac{\partial C_D}{\partial t_D} = \frac{\partial}{\partial x_D} \left( D \frac{\partial C_D}{\partial x_D} \right)$$

Dimensionless and dimensional diffusion equations are the form if the spatial and temporal scales are related by  $x_0^2 = t_0$  Typical for normal (Fickian) diffusion

For fractal objects, the mean-square displacement of a random walker depends on time as follows:

 $\langle x^2 \rangle \sim t^{2/(2+\theta)}$ 

 $\theta$ : index of anomalous diffusion ( $\theta$  = 0 normal diffusion)



**UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT** 

### **Physical & Mathematical Basis**

### **Anomalous Diffusion**

For normal diffusion 
$$\langle x^2 \rangle \sim t$$
 and  
Continuity Equation:  $\frac{\partial C}{\partial t} = -\frac{\partial}{\partial x} (J_C)$ 

$$J_C = -D\frac{\partial C}{\partial x}$$

For anomalous diffusion (the generalized case), the continuity equation, flux equation, or both should be modified to satisfy

$$\langle x^2 \rangle \sim t^{2/(2+\theta)}$$
 and  $\theta = 0 \implies$  normal diffusion



# **Modeling Anomalous Diffusion**

Option 1:

**Define**  $D(x) = D_{f\theta}x^{-\theta}$  **D**<sub>f</sub>e: effective coefficient of diffusion (constant)

Substitution into continuity equation yields

$$\frac{\partial C}{\partial t} = -\frac{\partial}{\partial x} \left( J_C \right) = \frac{\partial}{\partial x} \left( D_{f\theta} x^{-\theta} \frac{\partial C}{\partial x} \right)$$

In dimensionless form

$$\frac{x_0^2}{t_0^{2/(2+\theta)}} \frac{\partial C_D}{\partial t_D} = \frac{\partial}{\partial x_D} \left( D_{f\theta} x_D^{-\theta} \frac{\partial C_D}{\partial x_D} \right)$$

which satisfies the scale relation  $\langle x^2 \rangle \sim t^{2/(2+\theta)}$ 

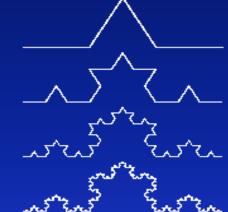
**UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT** 

### Modeling Approaches Option 1:

$$D(x) = D_{f\theta} x^{-\theta} \qquad \qquad \frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D_{f\theta} x^{-\theta} \frac{\partial C}{\partial x} \right)$$

The index of anomalous diffusion,  $\theta$ , is determined by the fractal dimension of the medium,  $d_{f}$ .

Example: For the Koch curve  $(d_f = \ln 4 / \ln 3)$ , triple increase in spatial scale creates 16-fold increase in temporal scale:



$$3^{2+\theta} = 16 \Longrightarrow 2 + \theta = 2\frac{\ln 4}{\ln 3} = 2d_f \Longrightarrow \theta = 2d_f - 2$$



# **Modeling Approaches**

Option 1:

$$D(x) = D_{f\theta} x^{-\theta} \qquad \qquad \frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D_{f\theta} x^{-\theta} \frac{\partial C}{\partial x} \right)$$

This approach has been used in petroleum engineering literature to model flow in naturally fractured media; e.g.,

$$\phi(r) \propto r^{d_f - d} \qquad k(r) \propto r^{d_f - d - d_w + 2}$$

Sahimi and Yortsos (1970), Chang and Yortsos (1990), Flamenco-Lopez and Camacho (2003), Camacho et al. (2008), Camacho et al. (2011), etc.

This approach has limitations when we do not have symmetry in the system, etc.



### **Modeling Approaches**

Option 2:

Let  $\beta = \theta + 1$  and define a flux proportional to the fractional gradient of concentration of order  $\beta$ 

$$J_C = -D_{f\beta} \frac{\partial^\beta C}{\partial x^\beta}$$

Then the dimensional and dimensionless forms of the continuity equation become

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D_{f\beta} \frac{\partial^{\beta} C}{\partial x^{\beta}} \right) \qquad \qquad \frac{x_0^{1+\beta}}{t_0} \frac{\partial C_D}{\partial t_D} = \frac{\partial}{\partial x_D} \left( D_{f\beta} \frac{\partial^{\beta} C_D}{\partial x_D^{\beta}} \right)$$

which satisfy  $\langle x^2 \rangle \sim t^{2/(2+\theta)}$ 

### Modeling Approaches Option 2:

The new diffusion equation

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D_{f\beta} \frac{\partial^{\beta} C}{\partial x^{\beta}} \right)$$

Note that

$$\frac{\partial}{\partial x} \left( \frac{\partial^{\beta}}{\partial x^{\beta}} \right) = \frac{\partial^{1+\beta}}{\partial x^{1+\beta}} = \frac{\partial^{2+\theta}}{\partial x^{2+\theta}}$$

The order of the spatial derivatives is larger than 2

More than 2 space boundary conditions is required (for  $\theta$ =0, it does not default to normal diffusion)



UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

# **Modeling Approaches**

Option 2:

To have physically meaningful boundary conditions, the order of the spatial derivative should be 2 or less

This imposes the requirement that  $\beta \leq 1$  in

$$J_C = -D_{f\beta} \frac{\partial^\beta C}{\partial x^\beta}$$

 $\beta$  < 1 : non-local spatial gradients (long-range interactions) To satisfy the scale relation,  $\langle x^2 \rangle \sim t^{2/(2+\theta)}$ 

the flux relation should also include a fractional temporal derivative (temporal non-locality, memory dependence)



**UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT** 

## **Modeling Approaches**

Option 2:

Let us define a new flux relation by

$$J_{C} = D_{f\gamma\beta} \,\partial_{t}^{1-\gamma} \left( \frac{\partial^{\beta} C}{\partial x^{\beta}} \right), \qquad 0 < \gamma, \quad \beta < 1$$

where the Caputo definition of the temporal and spatial fractional derivatives are given by

$$\partial_t^{\gamma} C = \frac{\partial^{\gamma} C}{\partial t^{\gamma}} = \frac{1}{\Gamma(1-\gamma)} \int_0^t (t-\xi)^{-\gamma} \frac{\partial C}{\partial \xi} d\xi$$
$$\partial_x^{\beta} C = \frac{\partial^{\beta} C}{\partial x^{\beta}} = \frac{1}{\Gamma(1-\beta)} \int_0^x (x-\xi)^{-\beta} \frac{\partial C}{\partial \xi} d\xi$$



### **Modeling Approaches**

Option 2:

With the new non-local flux, the continuity equation becomes

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left[ D_{f\gamma\beta} \partial_t^{1-\gamma} \left( \frac{\partial^\beta C}{\partial x^\beta} \right) \right]$$

The scale analysis yields

$$\frac{x_0^{1+\beta}}{t_0^{\gamma}} \frac{\partial C_D}{\partial t_D} = \frac{\partial}{\partial x_D} \left[ D_{f\gamma\beta} \partial_{t_D}^{1-\gamma} \left( \frac{\partial^{\beta} C_D}{\partial x_D^{\beta}} \right) \right] \rightarrow x_0^2 = t_0^{2\gamma/(1+\beta)}$$

 $\beta$  and  $\gamma$  should be such that the the scale relation is satisfied  $\langle x^2 \rangle \sim t^{2/(2+\theta)} \rightarrow 2+\theta = (1+\beta)/\gamma$ 



UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

# **Modeling Approaches**

Option 2:

Riemann-Liouville fractional integration & derivative of order  $\alpha$   $_{a}I_{t}^{\alpha}f(t) = \frac{1}{\Gamma(\alpha)}\int_{a}^{t}(t-\tau)^{\alpha-1}f(\tau)d\tau$  $_{a}^{n}D_{t}^{\alpha}f(t) = \frac{1}{\Gamma(n-\alpha)}\frac{d^{n}}{dt^{n}}\int_{a}^{t}(t-\tau)^{n-\alpha-1}f(\tau)d\tau$ 

Note that 
$$\partial_t^{\alpha} C = \frac{\partial^{-C} C}{\partial t^{\alpha}} = \frac{1}{\Gamma(1-\alpha)} \int_0^{-\alpha} (t-\xi)^{-\alpha} \frac{\partial C}{\partial \xi} d\xi = \frac{1}{0} D_t^{\alpha} C$$

and the fractional derivative is non-local (it is a convolution; it depends on the values of C(t) much farther away from t)

**UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT** 

# **Modeling Approaches**

Option 2:

Applying the Riemann-Liouville fractional integration to both sides of

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left[ D_{f\gamma\beta} \,\partial_t^{1-\gamma} \left( \frac{\partial^\beta C}{\partial x^\beta} \right) \right]$$

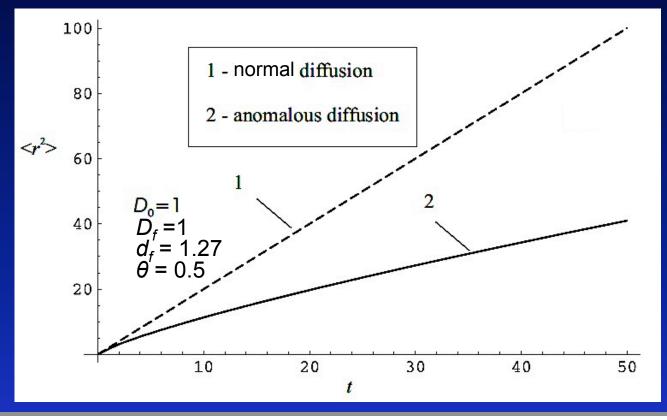
we obtain the common form of non-local, time-fractional, anomalous diffusion equation

$$\frac{\partial^{\gamma} C}{\partial t^{\gamma}} = \frac{\partial}{\partial x} \left( D_{f\gamma\beta} \frac{\partial^{\beta} C}{\partial x^{\beta}} \right)$$



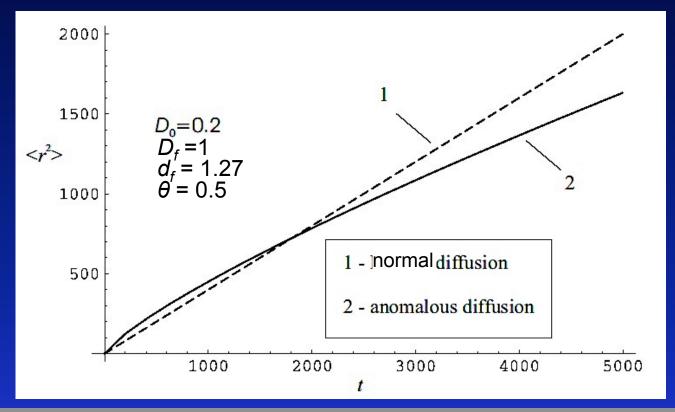
### **Non-Local Anomalous Diffusion**

Comparison of mean square displacement vs. time for normal and anomalous diffusion (Fomin et al., 2011)



### **Non-Local Anomalous Diffusion**

Comparison of mean square displacement vs. time for normal and anomalous diffusion (Fomin et al., 2011)



UNCONVEN Spring 2013

UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

#### **Implications of Anomalous Diffusion**

## **1D Normal Diffusion**

**Diffusive Flux** 

Continuity Equation):

$$J_C = -D\frac{\partial C}{\partial x}$$

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left( D \frac{\partial C}{\partial x} \right)$$

**Integer Derivative** 

$$\frac{\partial C}{\partial \xi} = \lim_{\Delta \xi \to 0} \frac{C(\xi + \Delta \xi) - C(\xi)}{\Delta \xi}$$

Definitions are straightforward BUT

Characterization is not very successful Matching the field data is not convincing



UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

#### **Implications of Anomalous Diffusion**

### **1D Non-Local Anomalous Diffusion**

**Diffusive Flux Continuity Equation):**  $J_{C} = D_{f\gamma\beta} \partial_{t}^{1-\gamma} \left( \frac{\partial^{\beta} C}{\partial x^{\beta}} \right) \qquad \qquad \frac{\partial^{\gamma} C}{\partial t^{\gamma}} = \frac{\partial}{\partial x} \left( D_{f\gamma\beta} \frac{\partial^{\beta} C}{\partial x^{\beta}} \right)$  $0 < \gamma$ ,  $\beta < 1$ **Fractional Derivative**  $\frac{\partial_{\xi}^{\gamma} C}{\partial_{\xi} C} = \frac{\partial^{\gamma} C}{\partial \xi^{\gamma}} = \frac{1}{\Gamma(1-\gamma)} \int_{0}^{\xi} (\xi - \xi')^{-\gamma} \frac{\partial C}{\partial \xi'} d\xi'$ 

Fractional derivatives are non-local and memory dependent



UNCONVENTIONAL RESERVOIR ENGINEERING PROJECT

### **Implications of Anomalous Diffusion**

## What is next?

How does this new perception change reservoir characterization and flow modeling?

$$J_{C} = D_{f\gamma\beta} \partial_{t}^{1-\gamma} \left( \frac{\partial^{\beta} C}{\partial x^{\beta}} \right), \quad \frac{\partial^{\gamma} C}{\partial t^{\gamma}} = \frac{\partial}{\partial x} \left( D_{f\gamma\beta} \frac{\partial^{\beta} C}{\partial x^{\beta}} \right) \qquad 0 < \gamma, \quad \beta < 1$$

How do you estimate a diffusivity coefficient (or permeability) which is defined by a non-local, memory dependent flux law?

How do we use data to determine the fractional powers of the temporal and spatial derivatives?

