



## Summary and Background

### PHASE BEHAVIOR IN NANOPOROUS MEDIA

- UREP Research Tasks on Phase Behavior
- Status of Tasks (with more details on T4 and T5)
- Vision for Integration
- Publications



## UREP research tasks on phase behavior

PROJECT 1 Flow and Transport of Hydrocarbon Fluids in Nano-Porous Reservoirs	Phase 3 Tasks	
	1. Understand trends in field data	Have not received any data to date
	2. Dew-point measurements in nanofluidic chips and comparison with models	} Asm Kamruzaman (PhD) Measurement of condensation in nanofluidics
	3. Effect of temperature on experiments	
	4. Core measurements	Keerthana Krishnan (MS) Capillary condensation in Niobrara
	5. Upscaling experimental results	Ran Gao (visiting student) Three-phase equilibrium models
	6. Molecular simulations	Yakup Coskuner (MS)



## Research tasks on phase behavior (T2 & T3)

### T2 – Sponsored by DOE STTR – Kaia Corp.

Phase behavior of  $C_3$  in nanofluidics

Comparison with Kelvin equation (had difficulties in matching)

Measure pressure change in the vicinity of phase change

### T3 – Asm Kamrruzaman

Repeat previous  $C_3$  experiments

Design pressure / temperature enclosures

Conduct nanofluidic experiments at different temperatures

Experiments with mixtures and compare with model

Green = Completed; Yellow = Current; White = Planned



## Research tasks on phase behavior (T4)

### T4 – Keerthana Krishnan

Capillary condensation of  $C_3$  in Niobrara

Capillary condensation of  $C_3$  in synthetic nanopores

Other rocks

Other gas or gas mixtures

Effect of water

Effect of crushing

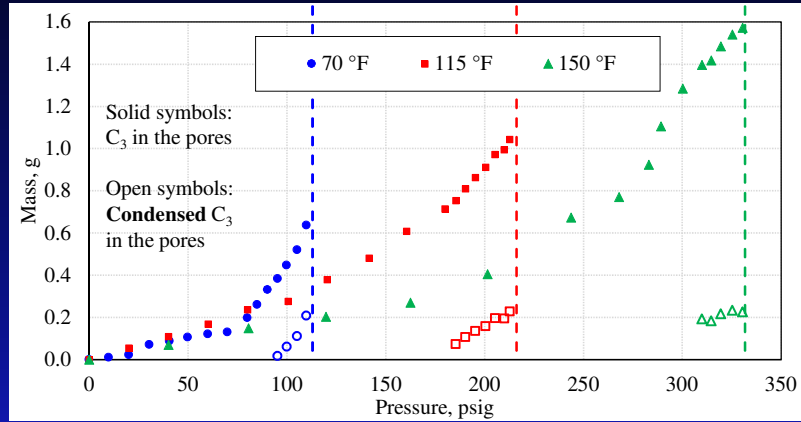
Compare with upscaled models (T5 – core level)



## Research tasks on phase behavior (T4)

### T4 – Main results

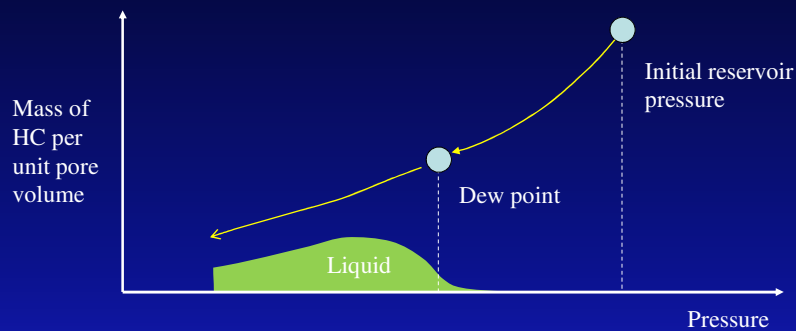
Capillary condensation of  $C_3$  in Niobrara



## Research tasks on phase behavior (T4)

### Plan for T4

Experimentation and model for HC in place that accounts for the effect of capillary condensation for condensate reservoirs



## Research tasks on phase behavior (T5)

### T5

Vapor-liquid phase behavior in a single pore

Vapor-liquid phase behavior in multiple pores (pore size distribution)

#### General multi-phase ( $\geq 3$ ) equilibrium

- Model constructed and validated using data from literature
- CO<sub>2</sub>-oil-water and C<sub>2</sub>-oil-water phase behavior measured
- Writing papers ...

Vapor-liquid-adsorption phase behavior

Upscale to the core level, considering equilibrium among pores of different sizes but no variation in pressure and temperature

#### Coz-Sim

Upscale to the reservoir level, considering pressure variations due to flow, and explain and predict field data (T1)



## T5 – Main results

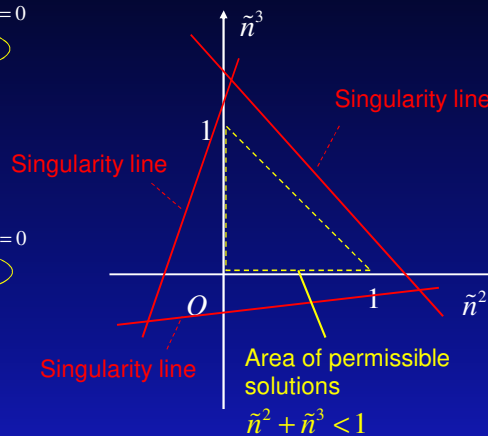
### 3-Phase equilibrium equations (Rachford-Rice)

$$\sum_{i=1}^{n_c} \frac{(1 - K_i^{12}) z_i}{K_i^{12} + (1 - K_i^{12}) \tilde{n}^2 - K_i^{12} \left(1 - \frac{1}{K_i^{13}}\right) \tilde{n}^2} = 0$$

Condition that the denominator = 0 gives a set of lines on which ①  $\rightarrow \pm \infty$

$$\sum_{i=1}^{n_c} \frac{(1 - K_i^{13}) z_i}{K_i^{13} + (1 - K_i^{13}) \tilde{n}^3 - K_i^{13} \left(1 - \frac{1}{K_i^{12}}\right) \tilde{n}^2} = 0$$

Eq. ② also has a set of singularity lines



## Solution procedure of multiphase equilibrium

Identify the singularity lines surrounding the area of permissible solutions

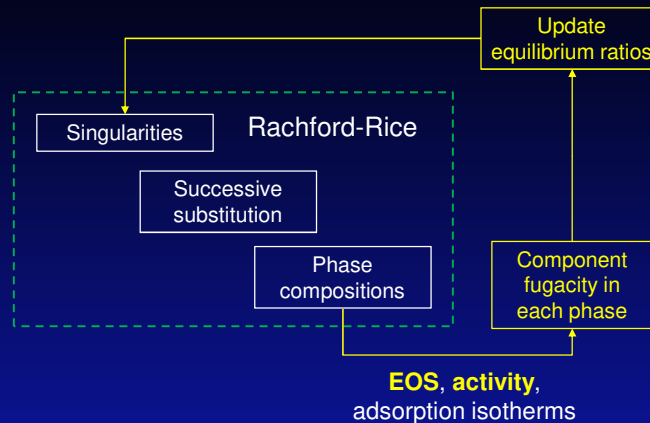
- This solution procedure is robust and is now extended to *N-phase flash*
- Solution is sought in an Euclidean space with dimension  $N - 1$
- Singularities are Euclidean sub-spaces with dimension  $N - 2$

Use successive substitution to solve Eq. (1) and (2) iteratively

Converged  $\tilde{n}^2$  and  $\tilde{n}^3$  are used to compute the compositions of the phases  $x_i^1$  through  $x_i^3$



## Incorporation of fugacity models



### Work completed

- EOS and activity models have been implemented
- Gas-oil phase behavior with water can now be done



### 3-Phase PVT measurements for verification

Gas: CO<sub>2</sub>, C<sub>2</sub>H<sub>6</sub>  
Liquid: Niobrara Oil, DI water  
Temperature = 215 F

Fluids	Bubble point
90% oil + 10% CO <sub>2</sub>	336 psig
90% oil + 10% C <sub>2</sub> H <sub>6</sub>	146 psig
0.2*(0.9*oil + 0.1*CO <sub>2</sub> ) + 0.8*water	182 psig
0.2*(0.9*oil + 0.1*C <sub>2</sub> H <sub>6</sub> ) + 0.8*water	165 psig

- C<sub>2</sub>H<sub>6</sub> is easier to dissolve in oil than CO<sub>2</sub>
- Water affects phase behavior of gas-oil systems
- CO<sub>2</sub>-oil system was affected more than C<sub>2</sub>H<sub>6</sub>-oil system



### Research tasks on phase behavior (T6 & T1)

#### T6

- Characterize bulk phase behavior of a pure substance
- Characterize confined phase behavior of a pure substance
- Characterize confined phase behavior of mixtures
- Compare with model (T5 - pore) and experiments (T2 and T3)

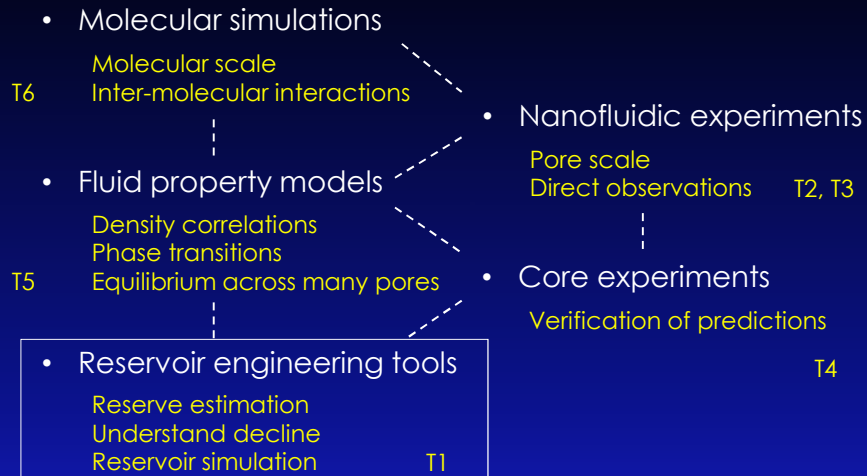
#### T1

- Acquire and analyze field data
- Use Coz-Sim to simulate field cases and compare (T5 – reservoir)

Green = Completed; Yellow = Current; White = Planned



## Phase behavior in nanopores – integration



## Phase behavior in nanopores – publications

- T1
  - Firingioglu et al. SPE 166459, 2013
- T2 & T3
  - Parsa et al. SPE 175118, 2015
- T4
  - Larson et al. *Measurement Sci. Tech.* (2017), 28:065902
  - Cho et al. on capillary condensation in Niobrara – under preparation
- T5
  - Firingioglu et al. SPE 159869, 2012
  - Teklu et al. *SPE Res. Eval. Eng.* (2014), 17:396
  - Wang et al. *SPE J.* (2016), 21:1981
  - Gao and Yin on modeling of multi-phase equilibrium – under preparation
  - Gao et al. on PVT of gas-oil-water phase equilibrium – under preparation
- T6
  - Coskuner et al. SPE 187163, 2017

